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1 **A Quantitative Failure Analysis on Capacity Fade in Rechargeable Lithium Metal**
2 **Cells**

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14 **Keywords:** Rechargeable lithium metal batteries; Lithium metal electrode; Charge
15 retention; Capacity fade; State of charge; Failure mode and effect analysis (FMEA)

19 **Abstract**

20 Rechargeable lithium battery (RLB) technology is transforming portable devices,
21 vehicle electrification, and grid modernization. To make RLB durable, reliable and safe,
22 conducting failure mode and effect analysis (FMEA) to identify failure mechanism under
23 the operating conditions is very desirable. However, this ability is often overlooked or
24 even lacking. The FA is often conducted by laboratory testing and postmortem analysis,
25 and the knowledge typically empirical. Here we present a quantitative approach for
26 FMEA that can reveal how failure modes and effects reduce the capacity of a RLB. This
27 approach is based on the state of the battery for FMEA, contrary to the conventional
28 approach based on operating or testing conditions. The key aspect of this FMEA method
29 is to convert the experimental results to a state-of-charge (SOC)-based analytic
30 methodology. Such a conversion can separate the thermodynamic and kinetic attributes of
31 capacity fade based on compositional correspondence in the electrode, so the loss and the
32 decreased utilization of the active materials can be determined respectively.

33 1 Introduction

34 Li metal electrode (LME) is considered the “holy grail” for high-energy rechargeable
35 Li batteries (RLB) designs that can surpass 350 Wh kg⁻¹ for electric vehicle applications
36 [1-4]. Yet, to date almost all possible designs encounter cycle life issues associated with
37 LME performance. The conventional approach to understand LME performance relies on
38 electrochemical testing of the cells. This approach measured capacity fade under various
39 experimental conditions and determine the cause of the fading by physicochemical
40 characterizations of the electrode materials. The results are empirical, and the lack of
41 quantitative correlation between the amount of capacity fade and the degree of severity
42 caused by the fading mechanism is prohibiting effective improvements to aid battery
43 performance today. A comprehensive, reliable analytic diagnosis on cell performance
44 using an electrochemical evaluation technique is highly desired to enable battery
45 researchers to understand the test results in order to improve their approach in solving
46 technical issues.

47 Although the underlying failure mechanisms associated with LME are known for some
48 time, and they are primarily due to the solid electrolyte interphase (SEI) formation that
49 consumes the electrolyte. In addition, excessive SEI formation could lead to isolation of
50 some Li metal into “inactive” or “dead Li.” The interplay of SEI and “dead Li” formation
51 caused the loss of Li inventory (LLI). More devastatingly, this process changed the
52 surface morphology and roughness of the LME significantly, as well as increased
53 porosity in the bulk of LME cycle by cycle. This vicious cycle also disturbed electrolyte
54 distribution in the cell and further increased the electrolyte depletion [3,5-8]. There is
55 little success to quantify these attributes to improve cycle life. To extend cycle life and
56 sustain reliable operation of these RLBs, there is an urgent need to identify and quantify
57 failure modes and effects on the performance of LME *in situ* and *operando* [9-15]. Here,
58 we introduce an accurate and precise “electrochemical analytic diagnosis (eCAD)”
59 method to determine the attributes and amount of capacity loss in LME-based RLB
60 during cycle aging. This method clearly identifies and quantifies capacity fade due to (1)
61 loss of active materials (LAM) and LLI (which are thermodynamic attributes) and (2)
62 under-utilization of the electrode active materials (UAM) due to rate-dependent
63 polarization (IR) and additional transport-related kinetic polarization hindrance (KPH)—
64 all kinetic attributes. This method offers a comprehensive comparison and data analytic
65 capability superior to the prior arts, such as those using incremental capacity analysis
66 (dQ/dV) or alike [8,16-19]. This approach emphasizes thermodynamic state
67 determination to derive accurate interpretation and inference of the experimental data
68 based on the state-of-charge (SOC) changes in the cell and the performance under the
69 influence of operating conditions. Such knowledge is very useful for developing proper
70 guidance to improve RLB design and operation. The knowledge gained from the

71 thermodynamic aspect should be more universal for the cell chemistry than those from
72 the kinetic aspects (that are sensitive to cell design metrics and dimensional scales that
73 extend from materials, electrodes, to cell). Since this approach is quantitative, a failure
74 mode can be identified and its effect on performance quantified. Furthermore, any
75 deviations observed in the operating or testing conditions can be easily aligned with the
76 performance metrics of the cell at a defined state. Such a thermodynamic state-based
77 failure mode and effect analysis (FMEA) on RLB functions is non-invasive and *in*
78 *operando*. The ability to quantify failure modes and effects as a function of the “state of
79 the system” is unique and beneficial for practical applications.

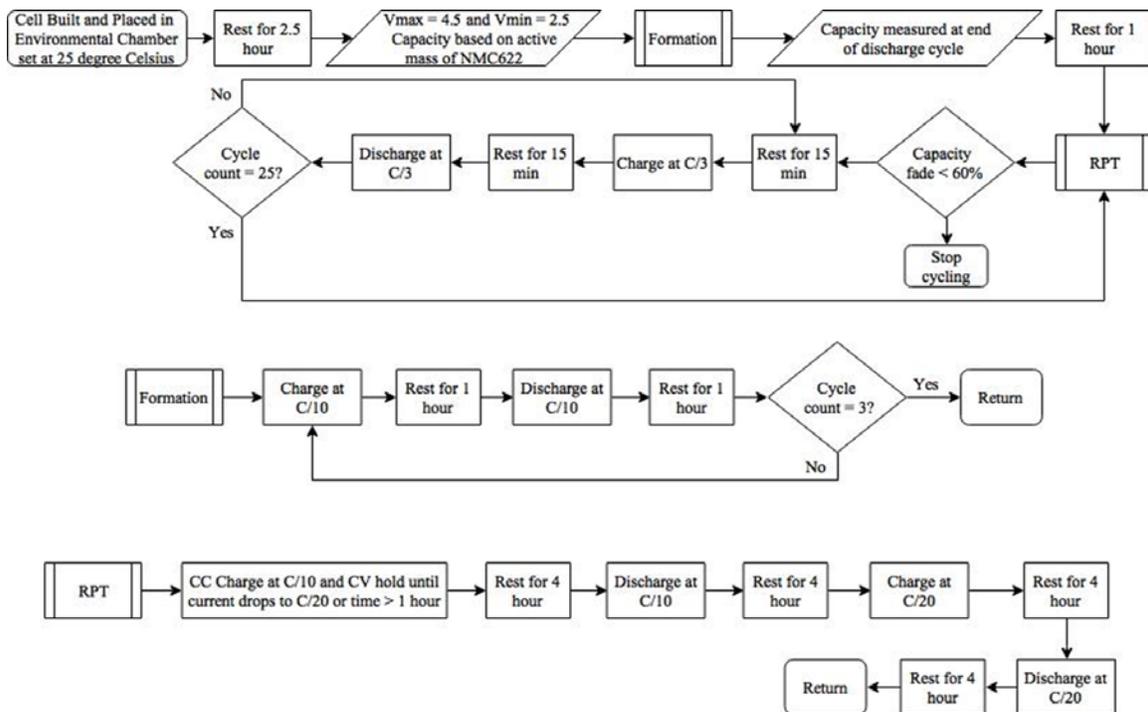
80 **2 Experimental**

81 **Cell Build:** Electrolyte was prepared by dissolving 1.2 M lithium hexafluorophosphate
82 (LiPF₆, Kishida) into a 3:7 (w/w) mixture of ethylene carbonate (EC, BASF) and ethyl
83 methyl carbonate (EMC, BASF) with 2 wt% vinylene carbonate (VC, BASF). The
84 positive electrode laminates were acquired from the Cell Analysis, Modeling and
85 Prototyping (CAMP) facility at Argonne National Laboratory (ANL). These laminates
86 were prepared from blend of 90% Li_xNi_{0.6}Mn_{0.2}Co_{0.2}O₂ (NMC-622) with 5% Timcal C45
87 carbon black and 5% polyvinylidene fluoride (PVDF) binder. The laminates were cast on
88 20 μm thick Al foil with a loading of 10.03 mg cm⁻² (including inactive components).
89 The calendared thickness and porosity of the laminate was 58 μm (1.45 mAh cm⁻² areal
90 capacity) and 35% (based on loading), respectively. The LME used was 250 μm thick Li
91 foil (MTI Corporation). Celgard 2500 was used as the separator, which is a porous
92 polypropylene membrane with 55% porosity.

93 Prior to assembly all the CR2032 components, spacers, and spring were washed with
94 ethanol in an ultrasonic bath for 15 minutes and dried at 60°C (at vacuum strength greater
95 than -75 kPa) for a minimum of 8 h prior to introduction into the glovebox. A 1.43 cm
96 diameter negative LME was punched from the Li foil and pasted on the spacer inside the
97 glovebox. A 1.43 cm diameter of cathode disk was punched from the NMC-622
98 laminates and dried at 90°C (at vacuum strength greater than -75 kPa) for a minimum of
99 8 h prior to use. The disks were carefully weighed after transferring to the glovebox. Full
100 cells of LME || NMC-622 in CR2032 coin-cell configuration were assembled inside an
101 Argon filled glovebox with H₂O and O₂ level held below 0.2 ppm. The cells were filled
102 with 14 μL electrolyte (5.8 g Ah⁻², ~3.16 times the total porosity in the separator and
103 cathode) in a single aliquot and sealed with Hoshen crimper.

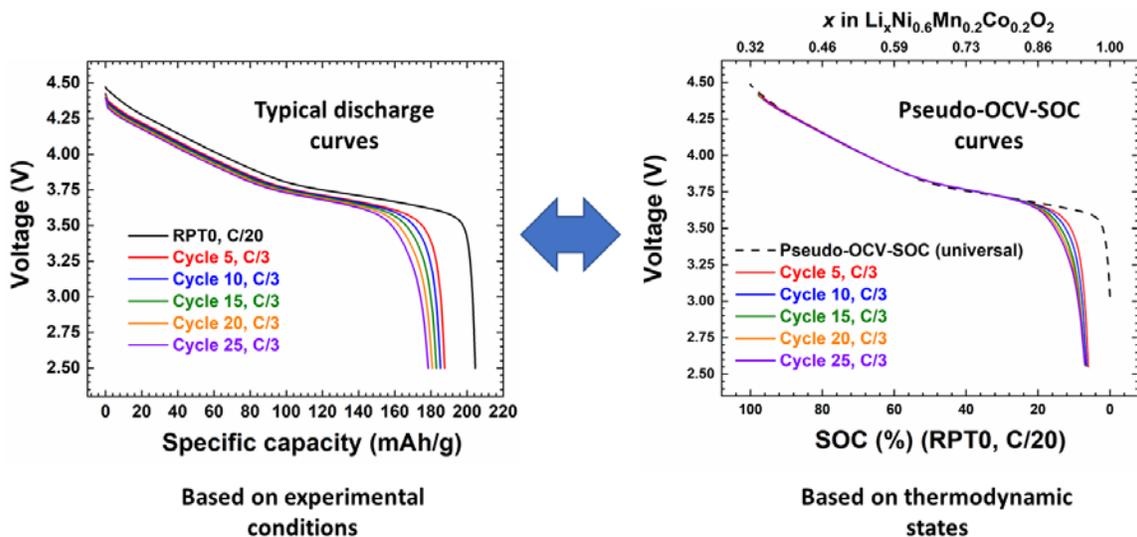
104 **Cycle Aging Test Protocol and Schedule:** The cells were cycled inside an environmental
105 chamber set at 25°C using either a Maccor 4000 or a Bio-Logic cyler between 2.5 V
106 (V_{min}) and 4.5 V (V_{max}). The testing protocol and schedule is shown in the flowchart in

107 Figure 1. The test schedule includes three formation cycles at C/10 rate. The capacity at
 108 the end of the third formation cycle was used as the nominal capacity of the cell. An
 109 initial Reference Performance Test (RPT-0) of the cell was conducted after the formation
 110 cycles. The RPT comprises one C/10 and one C/20 charge-discharge cycle to evaluate the
 111 utilization of the NMC cathode active material at these rates. Twenty five (25) charge-
 112 discharge cycles at C/3 for performance evaluation were commenced after RPT-0,
 113 followed by PRT-1. Such a schedule was continued every 25 cycles to determine the
 114 state-of-health of the cell and its capacity fade cycle by cycle.
 115



116
 117

Figure 1. Cycle aging test protocols and schedule.



118

119 Figure 2. The unique aspect of the electrochemical analytic diagnosis (eCAD) technique:
 120 the ability to transform (a) a series of discharge curves of an LME || NMC-622
 121 cell as a function of experimental conditions into (b) a series of thermodynamic
 122 state-of-charge (SOC) based analytic curves to reveal the attributes of the capacity
 123 fade during cycle aging.

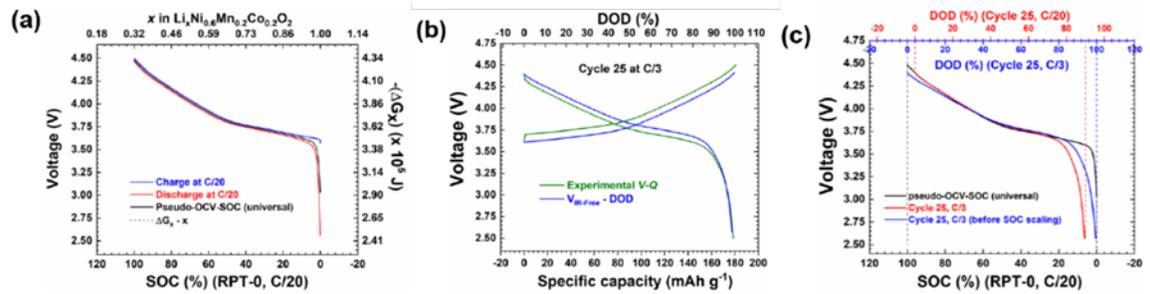
124 3 The Electrochemical Analytic Diagnosis (eCAD) Technique

125 The unique aspect of the electrochemical analytic diagnosis (eCAD) technique is
 126 shown in Figure 2. Typical discharge curves from cycle aging experiments of a LME ||
 127 NMC-622 coin cell at C/3 rate and 25°C are shown in Figure 2(a). Using this experiment
 128 as an example, we showed that these curves can be transformed into a series of SOC-
 129 based analytic discharge curves to display the changes of Li content in the NMC
 130 composition during cycle aging. The data transformation is illustrated in Figure 3.

131 3.1 Deriving SOC-Based Discharge Curves for Electrochemical Analytic 132 Diagnosis

131 The eCAD method is a thermodynamic state-based FMEA technique. Key to
 132 implement this eCAD method successfully is the use of thermodynamic states as the
 133 basis to properly infer the nature of the capacity fade in cycle aging. Such a basis is
 134 established by a well-defined correspondence between cell open circuit voltage (OCV)
 135 and SOC, which is universal without bias of size, shape, weight of the cell and other cell
 136 design metrics including geometric dimensions, active material loading of the electrodes,
 137 porosity and active surface area in each electrode, properties of the separator and binder,
 138 etc. [16-20]. This OCV–SOC correspondence is a direct representation of the Gibbs free
 139 energy of the cell reaction (denoted as $\Delta G_{\text{NMC-622}}$) and the Li content in the active

140 material's composition in the NMC-622 electrode; or, in a simplified notation as: ΔG_{x-x} ,
141 where x is the Li content in NMC-622 in the pseudo-binary Li-NMC-622 system
142 This universal relationship lays the foundation for inferring Li content in NMC-622,
143 as explained in a recent work by Li *et al.* [20]. Applying this principle in the eCAD
144 method to the LME || NMC-622 cell, the following steps are used in the transformation of
145 the analytic discharge curve:
146 Step 1) Derive the *pseudo*-OCV versus SOC curve from a set of charge discharge
147 curves at C/20 (as in RPT-0). The principle and method to derive the *pseudo*-OCV-SOC
148 curve has been described in prior work by Liaw and his co-workers [16-20], therefore we
149 do not explain further herein. It is worth noting that this OCV-SOC curve can also be
150 obtained by Galvanostatic Intermittent Titration Technique (GITT). However, prior study
151 indicated that the two methods should yield a very similar curve. Whereas the GITT
152 curve would be populated with and traced by only data points determined by the
153 experiments, this *pseudo*-OCV versus SOC curve obtained from the averaging of the
154 charging and discharging curves gives the full characteristic over the entire SOC range.
155 Thus, it is much more convenient and useful to use this averaging method of C/20
156 charging and discharging curves to yield the *pseudo*-OCV-SOC curve.
157 Step 2) Transform a typical discharge curve at C/3 into an IR-free voltage ($V_{IR-free}$)
158 versus specific capacity profile (a $V_{IR-free}-Q_{C/3}$ curve) and then further into a $V_{IR-free}$ versus
159 depth of discharge (DOD) profile (a $V_{IR-free}$ -DOD curve @C/3). Here, the effect of
160 polarization is removed as much as possible to attain an approximated state that is close
161 to the *pseudo*-OCV.
162 Step 3) Transform the $V_{IR-free}$ -DOD curve @C/3 into that @C/20 to correlate the
163 $V_{IR-free}$ -DOD curve @C/20 to the universal *pseudo*-OCV-SOC curve. Here, the capacity
164 measured in the experiment is mapped to DOD first and then aligned with SOC. Using
165 Cycle 25 discharge curve at C/3 in Figure 3(c) as an example, at the end of discharge
166 (EOD) the DOD is 100% at C/3. However, this $Q_{C/3}$ at 100% DOD is only 87.3% DOD
167 in $Q_{C/20}$.
168 This transformation of DOD from $Q_{C/3}$ to $Q_{C/20}$ allows us to align the curve with the
169 *pseudo*-OCV-SOC at any point in time through cycle aging to reveal the failure modes
170 and effects in the cell. This approach could also be applied to calendar aging studies with
171 RPTs. This process allows us decipher if a deviation in the cell performance is related to
172 (1) the Li content in the cathode (NMC-622) composition to determine the amount of
173 materials loss (LAM and/or LLI)—thermodynamic origins—or (2) UAM due to rate-
174 dependent IR or KPH as an attribute arisen from additional polarization effects at the
175 corresponding SOC as revealed by the $V_{IR-free}$ in the experiments—kinetic origins.
176

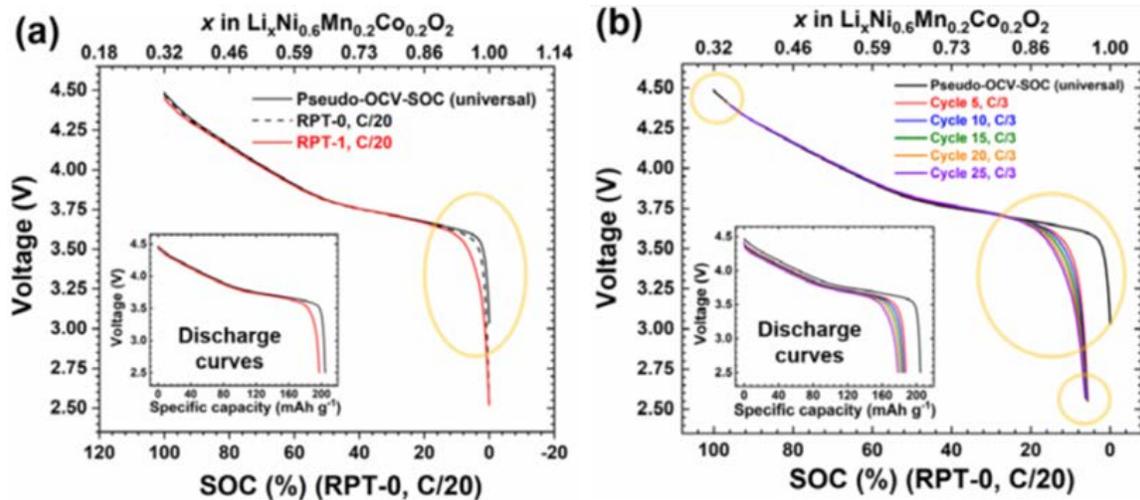


177

178 Figure 3. Schematic showing the steps involved in the FMEA analytics using the state of
 179 cell to analyze capacity fade in an LME || NMC-622 cell.

4 Understanding the FMEA on an LME || NMC-622 Cell

Figure 4 shows the capability of this thermodynamic state or SOC-based FMEA on a sample cell that behaved as anticipated from the cell design in the build. In Figure 4(a) the SOC-based analytic discharge curves from RPT-0 to RPT-1 along with the *pseudo*-OCV-SOC curve are shown and the variations displayed as highlighted by gold colored circular lines. Figure 4(b) further shows that, as the discharge rate increased from C/20 to C/3, additional UAM attributes to the capacity loss could be revealed.



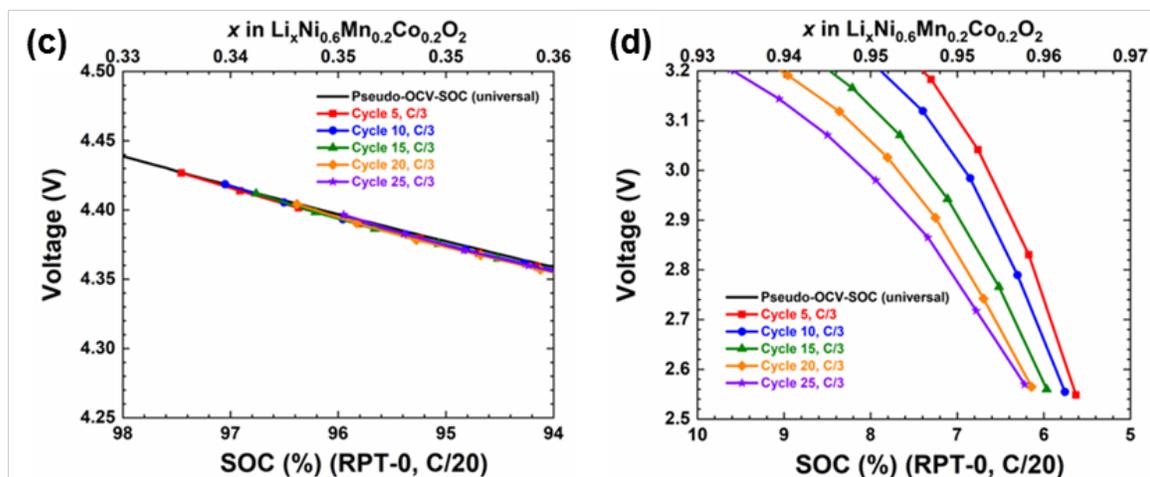


Figure 4. FMEA on an LME || NMC-622 cell for revealing rate dependent capacity fade (QF) during cycle aging. (a) State changes in two reference performance tests (RPT-0 to RPT-1, C/20). (b) Evolution of the state in five discharge regimes at C/3: Cycle 5, 10, 15, 20 and 25 over the cycle aging. The insets are the corresponding discharge curves for comparison. The areas, as highlighted by the circular translucent orange color in (b), are displayed in greater details in (c) beginning of discharge (BOD) and (d) end of discharge (EOD) where distinct features that reveal fading phenomena attributed to QF can be easily observed.

Table 1 provides more detailed information of the FMEA on the capacity fade (QF) and its attributes. The results are summarized as follows:

- a) $QF_{LAM@C/20}$ —The $Q_{C/20}$ fade from RPT-0 to RPT-1—is attributed to the loss of active material (LAM) in NMC-622 based on the following considerations:
 - i. The Li supply from LME is in significant excess in the cell build. There is no evidence to suggest that the Li supply was constrained in the first period of 25-cycle aging.
 - ii. As shown in Figure 4(a), the terminal compositions of NMC at the beginning of discharge (BOD) and EOD were almost identical in both RPTs. This result indicates the capacity came from the same compositional range in each test. Thus, if there were the same amount of NMC active material, we would expect to receive the same capacity. The difference in $Q_{C/20}$ from RPT-0 to RPT-1 therefore must be an active material loss.
 - iii. However, one can arguably saying that the SOC-based analytic discharge curves also indicated that KPH might have affected the utilization of NMC-622 (UAM) below 20% SOC. Therefore, we cannot rule out the possibility of KPH that could also attribute to the capacity fade at C/20 ($QF_{KPH@C/20}$). What

caused KPH cannot be concluded as yet, but a couple of usual suspects related to mass transport could be speculated. If so, QF_{KPH} could be recurring but unlikely accumulative.

- iv. Furthermore, based on the discussion below and Table 1, there are additional $QF_{IR@C/3}$ and $QF_{KPH@C/3}$ besides $QF_{LAM@C/20}$. If $QF_{LAM@C/20}$ were $QF_{KPH@C/20}$, then $QF_{KPH@C/3}$ and $QF_{KPH@C/20}$ would have very similar quantities, at least on the same order of magnitude. It is unlikely that QF_{KPH} is rate independent, especially between C/3 and C/20. Therefore, based on (iii) and (iv) we tend to rule out the possibility that $QF_{KPH@C/20}$ should account for $QF_{LAM@C/20}$.

On average $QF_{LAM@C/20}$ occurred on the order of 0.26 mAh g⁻¹ per cycle or 6.61 mAh g⁻¹ over the entire 25 cycles of C/3 aging (if the loss were not linear).

- b) $QF_{IR@C/3}$ —an ohmic dc resistance (IR drop)-induced capacity fade, an artifact due to rate-dependent UAM—is estimated on the order of 14.36 mAh g⁻¹ recurring in each cycle at C/3 for this cell. This quantity is estimated from the difference between the first cycle $Q_{C/3}$ and the $Q_{C/20}$ that was determined in RPT-0. Here we assume:
 - i. The ohmic dc resistance of the cell is rather constant over the SOC range studied in the cycle aging. This series resistance should include all conductive parts associated with the electrical current in the solids along the cell reaction pathway and the ionic current in the bulk electrolyte and in most cases in the electrode's porous media. We should note that the data acquisition rate and the slew rate of the tester's power electronics could affect the precision of the measurements, and we have paid attention to such issues in our analyses.
 - ii. At this stage of life, the morphology and electrode architecture of the NMC-622 cathode should not alter significantly to affect the electrode kinetics or mass transport in the pore structure of the cathode.
 - iii. Likewise, the morphology of LME and Li deposition and stripping rates also stay relatively stable in the first period of 25-cycle aging for the cell.
- c) $QF_{KPH@C/3}$ —an additional under-utilization of the NMC-622 cathode due to C/3 cycle aging—additional capacity fade on an order of magnitude similar to $QF_{LAM@C/20}$ but cannot be accounted for by the previous two origins. This quantity increases with cycle number in a linear fashion in the first period of 25-cycle aging, as shown in Table 1. It is also worth noting that $QF_{KPH@C/3}$ does change the terminal SOC at EOD cycle by cycle, unlike $QF_{LAM@C/20}$ which does not.

QF attributes (a)–(c) are consistent with the results exhibited in Figure 4(b), where the cathode utilization near the end of discharge (below 30% SOC) began to show the toll of KPH as the rate increased from C/20 to C/3 and cycle by cycle, where QF_{LAM} and QF_{KPH} , increase with cycle number. The sum of these losses as shown in the charge retention curve is rather linear.

Table 1. Detailed capacity fade attributes quantified by the FMEA from RPT-0 to RPT-1.

Cycle	Capacity (Q)	Loss of active material (QF_{LAM})	IR-induced UAM (QF_{IR})	KPH-induced UAM (QF_{KPH})
RPT-0 (C/20)	204.52	0.00	—	—
Cycle 1	189.90	0.26	14.36	0.00
Cycle 5	187.61	1.32	14.36	1.24
Cycle 10	185.31	2.64	14.36	2.21
Cycle 15	183.02	3.97	14.36	3.18
Cycle 20	180.81	5.29	14.36	4.07
Cycle 25	178.51	6.61	14.36	5.04
RPT-1 (C/20)	197.38	7.14	—	—
Cycle 26	177.15	7.32	14.36	5.70
Cycle 30	175.28	8.02	14.36	6.86
Cycle 35	172.99	8.90	14.36	8.28
Cycle 40	170.44	9.78	14.36	9.95
Cycle 45	168.23	10.67	14.36	11.27
Cycle 50	166.27	11.55	14.36	12.35
RPT-2 (C/20)	192.62	11.90	—	—

Note: all quantities in Q or QF are in mAh g⁻¹.

Two unique aspects of this FMEA approach should be noted here:

- a) The point-to-point detection of deviations in $V_{IR-free}$ as a function of SOC in the course of cell reaction is a consistent and reliable assessment of Li content in the NMC-622 cathode. This capability offers the basis for a clear identification of all capacity fade attributes and may offer the possibility to determine the Li inventory in LME, NMC cathode, and SEI formation with the electrolyte.
- b) This FMEA method applies thermodynamic principles to providing a reliable framework for accurate and precise fault detection in a quantitative manner.

5 Conclusion

We have shown the charge retention performance of a rechargeable Li metal cell and its cycle aging behavior. We used this sample cell to illustrate a quantitative failure mode and effect analysis (FMEA) based on thermodynamic state determination. Precise and accurate FMEA was demonstrated by true state-of-charge (SOC) correspondence and quantitative analysis of capacity fade (QF) attributes. These QF attributes include those from (1) the loss of active materials in the cathode (QF_{LAM}), (2) IR-induced, rate-

dependent under-utilization of capacity (Q_{FIR}), and (3) constrained transport-induced kinetic polarization hindrance that leads to increased under-utilization of the active material (Q_{FKPH}) in the cathode. A reliable FMEA has been achieved to show the potential of this electrochemical analytic diagnosis method for guarding reliable and safe battery operation with the ability to monitor capacity fading attributes quantitatively.

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Figure Captions

Figure 1. Cycle aging test protocols and schedule.

Figure 2. The unique aspect of the electrochemical analytic diagnosis (eCAD) technique: the ability to transform (a) a series of discharge curves of an LME || NMC-622 cell as a function of experimental conditions into (b) a series of thermodynamic state-of-charge (SOC) based analytic curves to reveal the attributes of the capacity fade during cycle aging.

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Table Captions

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